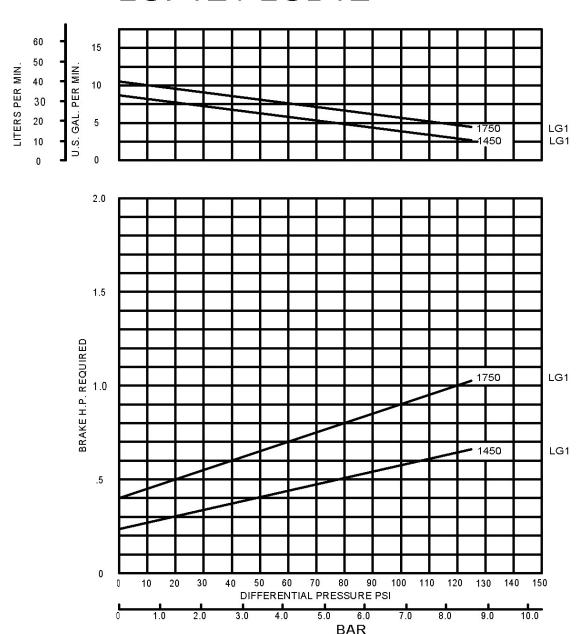


# CHARACTERISTIC CURVES LG, LGL and TLGL Series Pumps

Page Number	501-021
Effective	Feb 2021
Replaces	June 2010
Section	501

(as a stand-alone Curve page see 501-021a)

### LGF1E / LGB1E



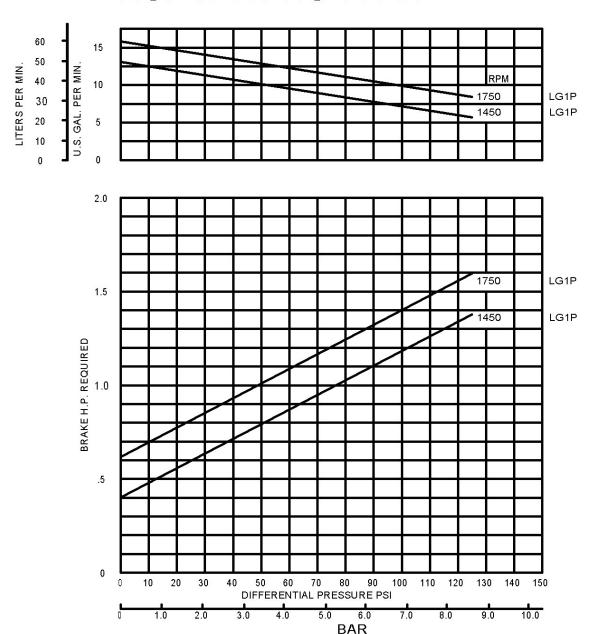
**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at  $80^{\circ}F$  (26.7°C). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at  $32^{\circ}F$  (0°C), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at  $80^{\circ}F$  (26.7°C) will be 60 to 70% of these values, and may run as low as 35 to 45% at  $32^{\circ}F$  (0°C). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.

### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021b)

## LGF1PE / LGB1PE



**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

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### LG, LGL and TLGL Series Pumps

2

20

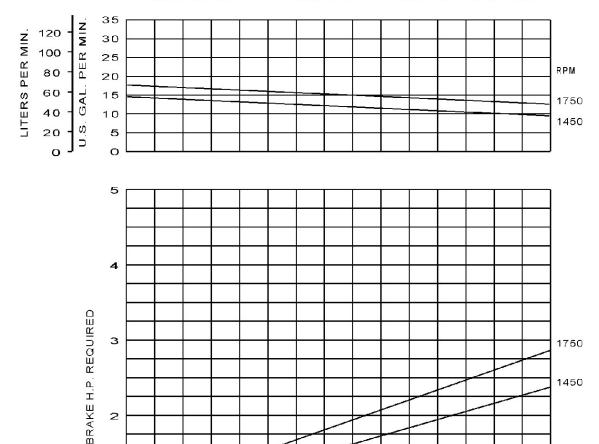
1.0

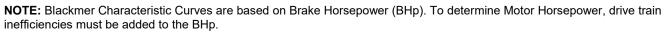
30

2.0

(as a stand-alone Curve page see 501-021c)

## LGRLF1.25A / LGRL1.25





60

50

70

DIFFERENTIAL PRESSURE PSI

80

90

6.0

100 110 120 130 140 150

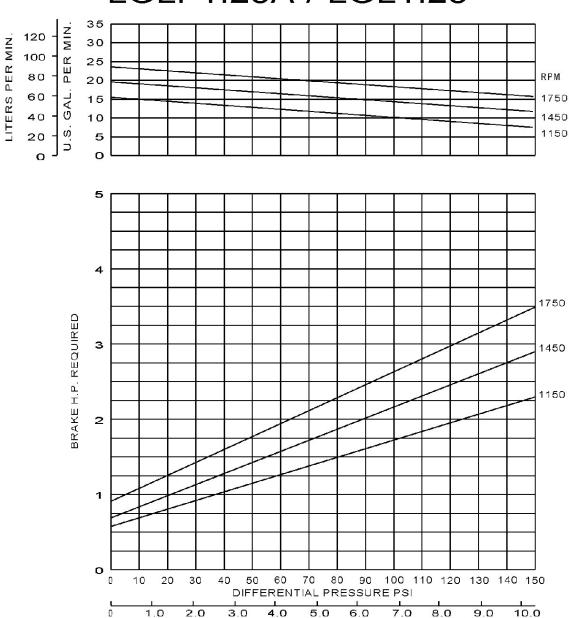
These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at 80°F (26.7°C). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at 32°F (0°C), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at 80°F (26.7°C) will be 60 to 70% of these values, and may run as low as 35 to 45% at 32°F (0°C). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.



### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021d)

## LGLF1.25A / LGL1.25



**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

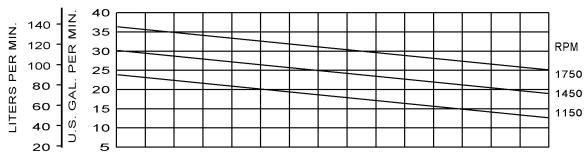
These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at  $80^{\circ}F$  ( $26.7^{\circ}C$ ). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at  $32^{\circ}F$  ( $0^{\circ}C$ ), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at  $80^{\circ}F$  ( $26.7^{\circ}C$ ) will be 60 to 70% of these values, and may run as low as 35 to 45% at  $32^{\circ}F$  ( $0^{\circ}C$ ). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.

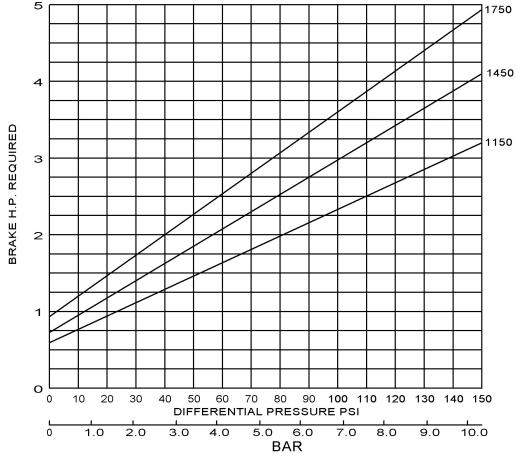


### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021e)







**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

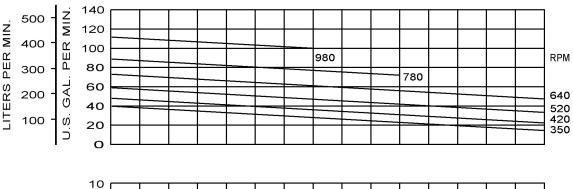
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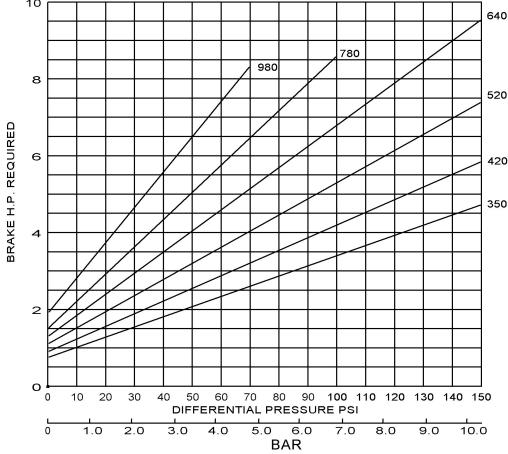


### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021f)

## LGLD2E / LGL2E





**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

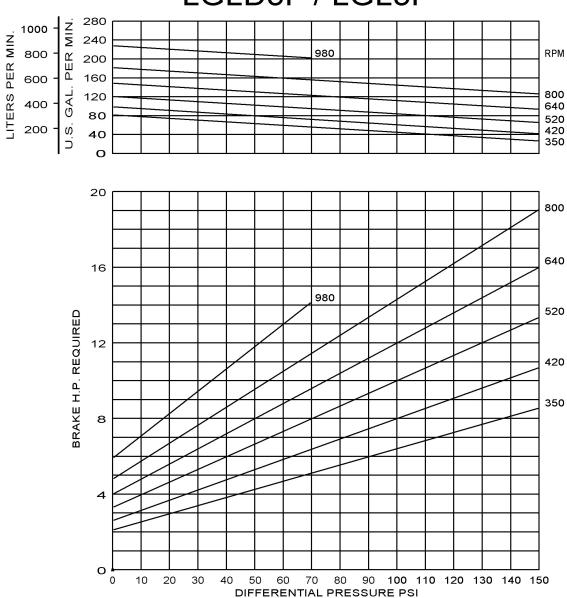
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### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021g)

## LGLD3F / LGL3F



**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

4.0

5.0

6.0

BAR

8.0

2.0

3.0

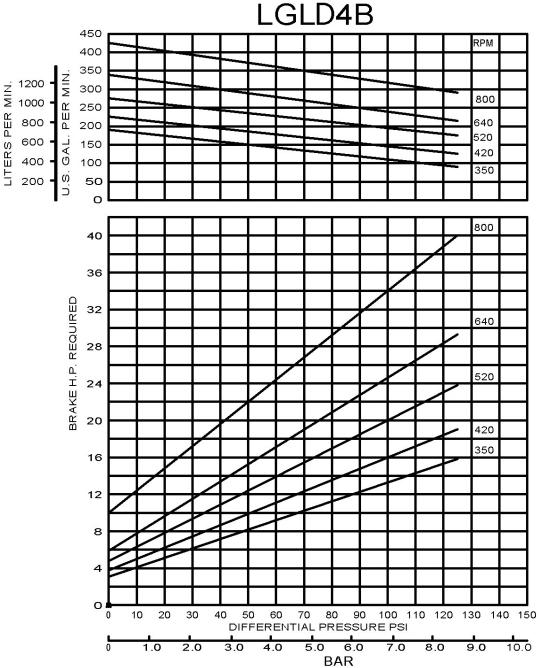
These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at 80°F (26.7°C). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at 32°F (0°C), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at 80°F (26.7°C) will be 60 to 70% of these values, and may run as low as 35 to 45% at 32°F (0°C). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.



10.0

### LG, LGL and TLGL Series Pumps





See next page for LGL4B

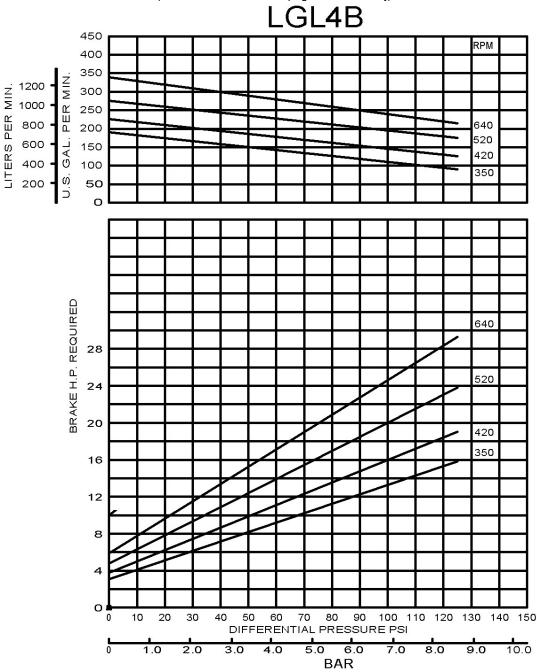
**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

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### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021j)



See previous page for LGLD4B

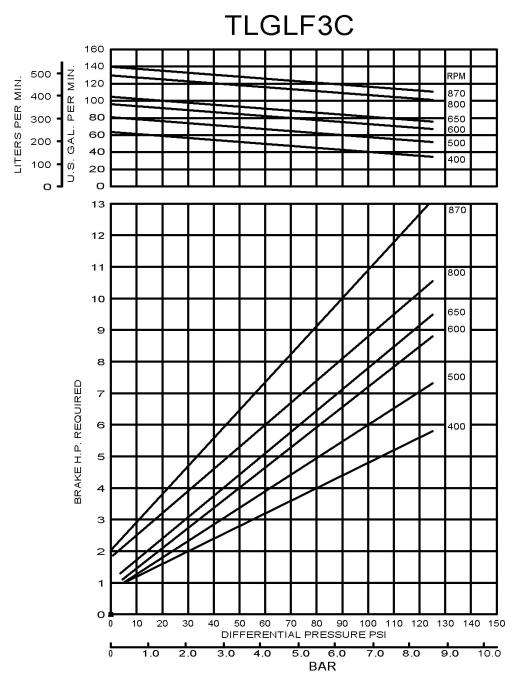
**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at 80°F (26.7°C). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at 32°F (0°C), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at 80°F (26.7°C) will be 60 to 70% of these values, and may run as low as 35 to 45% at 32°F (0°C). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.



### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021k)



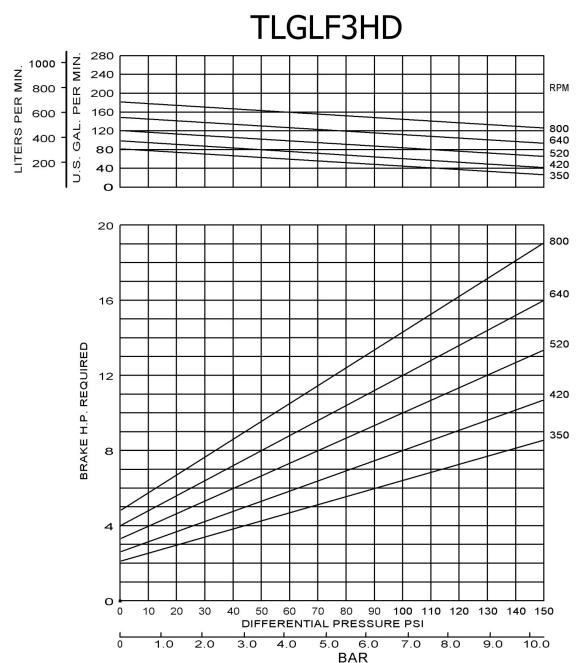
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These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at 80°F (26.7°C). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at 32°F (0°C), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at 80°F (26.7°C) will be 60 to 70% of these values, and may run as low as 35 to 45% at 32°F (0°C). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.



### LG, LGL and TLGL Series Pumps

(as a stand-alone Curve page see 501-021m)



**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

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### LG, LGL and TLGL Series Pumps

**NOTE:** Blackmer Characteristic Curves are based on Brake Horsepower (BHp). To determine Motor Horsepower, drive train inefficiencies must be added to the BHp.

3.0

These curves are based on approximate delivery rates when handling propane or anhydrous ammonia at 80°F (26.7°C). Line restrictions such as excess flow valves, elbows, etc., will adversely effect deliveries. For propane at 32°F (0°C), actual delivery will be further reduced to about 80% of nominal. Delivery of butane at 80°F (26.7°C) will be 60 to 70% of these values, and may run as low as 35 to 45% at 32°F (0°C). This loss of delivery is not a pump characteristic but is caused by natural thermodynamic phenomena of liquefied gases.

60 70 80

4.0

DIFFERENTIAL PRESSURE PSI

5.0

90

6.0

BAR

100 110 120

8.0

9.0

7.0



O

10 20 30

1.0

2.0

10.0